Beer's law over a range in concentration suitable for colorimetric analysis. The sensitivity, optimum experimental conditions and the effect of various ions have been determined. Best results were obtained with a 0.05% reagent solution and a nickel concentration of ten mg. per liter. The reagent will detect one part of nickel in 125 million parts of solution, when the observation is made in a 50-ml. (210-mm.) Nessler tube. The color develops satisfactorily in sulfuric acid solution up to approximately 0.002 normal. Traces of alkali cause fading. Many metallic ions give color reactions with the reagent and hence will interfere with the nickel determination unless they are removed. Iron and cobalt are the ions most likely to interfere and must be removed unless the nickel concentration is at least a hundred times greater than that of these ions.

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[CONTRIBUTION FROM THE FRICE CHEMICAL LABORATORY OF PRINCETON UNIVERSITY] THE HOMOGENEOUS COMBINATION OF ETHYLENE AND HYDROGEN. A SECOND-ORDER ASSOCIATION REACTION

> BY ROBERT N. PEASE Received January 4, 1932 Published May 7, 1932

It has recently been shown that the polymerization of ethylene at pressures above one atmosphere is a second-order homogeneous gas reaction.¹ The primary action is thus of the association type. In view of the fact that many homogeneous dissociation reactions are known to be first order, it was inevitable that second-order homogeneous association reactions should occur, unless the classical principle of mobile equilibrium is incorrect as ordinarily applied. Nevertheless, a theoretical difficulty has arisen in this connection which makes it especially desirable to investigate other cases. The hydrogenation of ethylene is a particularly suitable example since the reaction is reversible,² and the reverse action (dissociation of ethane) has been rather definitely shown to be first order.³

The theoretical difficulty mentioned above has to do with the accommodation of energy in a single product molecule newly formed by the collision of two reactant molecules. A rather crude analogy on a large scale is the cohesion of two "sticky" masses—say, two balls of tar—which have been directed at each other. In the latter case, any kinetic energy which is lost, and the cohesion energy are converted into internal energy of the resulting mass. Similarly in the case of two associating molecules, the

¹ Pease, THIS JOURNAL, **53**, 613 (1931). At lower pressures there is evidence of deviation. See Pease, *ibid.*, **52**, 1158 (1930). The polymerization of acetylene may also be second order. See Pease, *ibid.*, **51**, 3470 (1929).

² Pease and Durgan, *ibid.*, 50, 2715 (1928).

³ Marek and McCluer, Ind. Eng. Chem., 23, 878 (1931); Frey and Smith. ibid., 20, 948 (1928).

product molecule is called upon to accommodate in internal degrees of freedom any loss of kinetic energy due to the inelastic nature of the collision, plus the reaction energy, and the internal energies of the original molecules. However, since internal degrees of freedom are in general quantized, the chance that the product molecule should be able to do this appears to be negligible. The association is, therefore, extremely improbable.

The solution of this apparent difficulty was suggested by Kassel.⁴ The above argument implies that the internal degrees of freedom must be quantized *immediately* the molecule is formed. This cannot be assumed. Rather, the uncertainty principle indicates that the energies of individual states may differ from their final values by as much as $h/\Delta t$, where Δt is the time from the instant of collision. Therefore, if the total energy levels are spaced sufficiently closely, any value of the energy may be temporarily accommodated by the product molecule. Eventually, of course, any excess of energy over that exactly corresponding to some particular set of energy levels must be converted into kinetic energy in another collision, if the product molecule is to be stabilized.

The simplest reaction mechanism appears to be essentially that suggested by Taylor for the ethylene polymerization.⁵ Two molecules whose joint energy exceeds some minimum may unite on collision. The resulting quasimolecule may subsequently either dissociate spontaneously, or it may be dissociated as a result of a collision, or, finally, it may be stabilized as a result of a collision. Which of the last two happens will depend on the state of the molecule at the instant of collision. The rate of association will be

$\alpha Z_0 e^{-E/RT} c_1 c_2$

where α is an orientation factor, Z is the total collision rate at unit concentrations and E is the activation energy. If most quasi-molecules of products survive to undergo a collision (instead of decomposing spontaneously), the observed reaction rate will then be given by

$\alpha\beta z_0e^{-E/RT}c_1c_2$

where β is the fraction of subsequent collisions in which the quasi-molecule is stabilized, rather than decomposed. In the case of ethylene polymerization the product $\alpha\beta$ was found to be about 1/2000. As will be shown later, it is more nearly unity for the hydrogenation of ethylene.

Apparatus and Method

The apparatus and method were standard. The reaction was followed by measuring the pressure decrease at constant volume in a heated Pyrex reaction vessel of 500 cc. volume. After a measurement was completed, the reaction mixture was collected with a Töpler pump and analyzed.

⁴ Kassel, This Journal, 53, 2143 (1931).

⁵ Pease, *ibid.*, **53**, 613 (1931).

The hydrogen was purified by passage over hot platinized asbestos, and through a trap at -79° . The ethylene was purified by fractionation. Both gases were originally better than 99% pure.

Results

The experiments were subject to two limitations. Owing to simultaneous polymerization of ethylene, it was necessary to confine the measurements to mixtures containing a 3:1 excess of hydrogen. Satisfactory results were then obtained when the reaction vessel was unpacked. When, however, the vessel was filled with broken glass, it was found that considerable quantities of hydrogen were absorbed by the latter.⁶ As a result, the observed pressure decrease (at 550°) was about twice that with the empty vessel. Analysis of the gas reaction mixture after exposure showed clearly that the rate of ethane formation was normal. This is the more interesting since it shows that the absorbed hydrogen is not reactive.

The values of k_2 were calculated by means of the equation

$$k_2 = \frac{2.303}{t(a-b)} \log_{10} \frac{b(a-x)}{a(b-x)}$$

where t is the time in seconds, a is the initial pressure of hydrogen, b is the initial pressure of ethylene and x is the pressure of ethane at time t. In calculating values of k_2 , the first measurement (t = 300) was taken as the initial state.

Since the reaction is reversible, it was necessary to determine whether the reverse action was interfering to an appreciable extent. It was found that the values of k_2 were not appreciably different when the much more elaborate expression involving the rate of the reverse action was employed. Measurements were only carried up to 50% conversion of the ethylene.

The results of a series of experiments with $3H_2:1C_2H_4$ mixtures carried out in the unpacked reaction vessel are presented in Table I. It will be seen that the values of k_2 are reasonably constant at each temperature. At 550° measurements were made with initial total pressures of one, one-half and one-fourth atmosphere. Although the constants at one-half atmosphere were somewhat lower than the others, there is no reason to doubt that the reaction is second-order.

It has already been mentioned that polymerization of ethylene interfered when the reaction mixture contained more than 25% of this gas. This is shown by the data of Table II. Two runs were made at 550° with mixtures of $2H_2:1C_2H_4$ and $1H_2:1C_2H_4$. In each case the amount of hydrogen reacting was nearly the same as the amount of ethane formed. The amount of ethylene reacting exceeded this latter by 11% with the $2H_2:1C_2H_4$ mixture, and by 33% in the $1H_2:1C_2H_4$ mixture. In consequence it is not possible to calculate a constant for the formation of ethane. Ap-

⁶ Compare Alyea, THIS JOURNAL, 53, 1324 (1931).

TABLE I

RATES WITH 3H2:1C2H4 MIXTURES IN EMPTY REACTION TUBE

Initial press. H2, mm.573575580562294141Initial press. CrH4, mm.19519619819110048Initial total press., mm.768771778753394189Time,Obs.Obs.Obs.Obs.Obs.Obs.Obs.Obs.sec.press. kay 107press. kay 107press. kay 107press. kay 107press. kay 107press. kay 107300762766747717380183600758(1.3)7492.437335.3968515.137113.4180(19)900755(1.1)7432.257205.5066115.136313.61781612007521.087372.247095.42Av.15.135613.61761518007470.997252.316065.3734513.41721627007390.987082.406675.40Av.13.51681536007320.956932.47Av.5.42Av.13.51681536007321.016802.51720Av.13.51681513.41721627007031.01Av.2.37Av.5.42Av.13.52492145007231.01680 <td< th=""><th>Temp., °C.</th><th></th><th>4</th><th>75</th><th>50</th><th>00</th><th>52</th><th>4</th><th>55</th><th>2</th><th>548</th><th>3</th><th>550</th></td<>	Temp., °C.		4	75	50	00	52	4	55	2	548	3	550
Initial press. C2H4, mm.19519619819110048Initial total press., mm.768771778753394189Time, sec.Dbs. press. $k_2 \times 10^7$ Obs. press. $k_2 \times 10^7$ IsoIsoIsoIsoIsoIsoIsoIsoIsoIsoIsoIsoIsoIsoIsoIsoIsoIsoIso	Initial press. H ₂ , mm. Initial press. C ₂ H ₄ , mm.		5	573 195		575 196		580 198		562 191		294 100	
Initial total press., mm.768771778753394189Time, sec. press. $k_2 \times 10^7$ Obs. press. $k_2 \times 10^7$ Obs. press. 			. 1										
Time, sec.Obs. press	Initial total pres	s., mm	. 7	68	77	71	77	8	75	3	394		189
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	Time, sec.	Obs. press.	k₁×107	Obs. press.	k₂×107	Obs. press.	k₂×107	Obs. press.	k ₂ ×107	Obs. press.	k₂×107	Obs. press.	k ₂ ×107
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	300	762		756		747		717		380		183	
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	600	758	(1.3)	749	2.43	733	5.39	685	15.1	371	13.4	180	(19)
1200 752 1.08 737 2.24 709 5.42 Av. 15.1 356 13.6 176 15 1800 747 0.99 725 2.31 690 5.37 345 13.4 172 16 2700 739 0.98 708 2.40 667 5.40 Av. 13.5 168 15 3600 732 0.95 693 2.47 Av. 5.42 Av. 16 15 3600 732 1.01 680 2.51 7200 703 1.01 Av. 2.37 7200 703 1.01 Av. 2.37 Av. 16 4500 723 1.01 Av. 2.37 Av. 16 7200 703 1.01 Av. 2.37 Av. 16 C2H3 formed, mm. 65 91 111 92 49 21 C2H4 used, mm. 64 92 119 108 58 28 C3H4 used, mm. 69 96 124 <td>900</td> <td>755</td> <td>(1.1)</td> <td>743</td> <td>2.25</td> <td>720</td> <td>5.50</td> <td>661</td> <td>15.1</td> <td>363</td> <td>13.6</td> <td>178</td> <td>16</td>	900	755	(1.1)	743	2.25	720	5.50	661	15.1	363	13.6	178	16
1800 747 0.99 725 2.31 690 5.37 345 13.4 172 16 2700 739 0.98 708 2.40 667 5.40 Av. 13.5 168 15 3600 732 0.95 693 2.47 Av. 5.42 Av. 16 4500 723 1.01 680 2.51 720 703 1.01 Av. 2.37 Av. 1.00 Av. 2.37 Av. 16 Final press. change, mm. 65 91 111 92 49 21 CaH4 formed, mm. 64 92 119 108 58 28 CaH4 used, mm. 60 87 107 89 47 24 Hu used, mm. 69 96 124 112 62 25	1200	752	1.08	737	2.24	709	5.42	Av.	15.1	356	13.6	176	15
2700 739 0.98 708 2.40 667 5.40 Av. 13.5 168 15 3600 732 0.95 693 2.47 Av. 5.42 Av. 16 16 4500 723 1.01 680 2.51 Av. 1.0 16 16 7200 703 1.01 Av. 2.37 Av. 1.00 111 92 49 21 Final press. change, mm. 65 91 111 92 49 21 C ₂ H ₄ formed, mm. 64 92 119 108 58 28 C ₂ H ₄ used, mm. 60 87 107 89 47 24 H ₄ used, mm. 69 96 124 112 62 25	1800	747	0.99	725	2.31	690	5.37			345	13.4	172	16
3600 732 0.95 693 2.47 Av. 5.42 Av. 16 4500 723 1.01 680 2.51 7	2700	739	0.98	708	2.40	667	5.40			Av.	13.5	168	15
4500 723 1.01 680 2.51 7200 703 1.01 Av. 2.37 Av. 1.00 50 91 111 92 49 21 Calls formed, mm. 65 91 111 92 49 21 Calls formed, mm. 64 92 119 108 58 28 Calls used, mm. 60 87 107 89 47 24 Hu used, mm. 69 96 124 112 62 25	3600	732	0.95	693	2.47	Av.	5.42					Av.	16
7200 703 1.01 Av. 2.37 Av. 1.00 Final press. change, mm. 65 91 111 92 49 21 CaHs formed, mm. 64 92 119 108 58 28 CaHs formed, mm. 60 87 107 89 47 24 Ha used, mm. 69 96 124 112 62 25	4500	723	1.01	680	2.51								
Av. 1.00 Final press. change, mm. 65 91 111 92 49 21 CaHs formed, mm. 64 92 119 108 58 28 CaHs formed, mm. 60 87 107 89 47 24 Ha used, mm. 69 96 124 112 62 25	7200	703	1.01	Av.	2.37								
Final press. change, mm.6591111924921 C_2H_3 formed, mm.64921191085828 C_2H_4 used, mm.6087107894724Ha used, mm.6996i241126225		Av.	1.00										
C2H3 formed, mm. 64 92 119 108 58 28 C2H4 used, mm. 60 87 107 89 47 24 Ha used, mm. 69 96 124 112 62 25	Final press. change, mm.		บ.	65		91		111		92		49	
C2H4 used, mm. 60 87 107 89 47 24 Ha used, mm. 69 96 124 112 62 25	C2H1 formed, mm.			64		92		119		108		58	
H ₁ used, mm. 69 96 124 112 62 25	C2H4 used, mm.			60		87		107		89		47	
	H1 used, mm.			69	ç	96	12	4	112	2	62		25

TABLE II

AND 1H2:1C2H4	MIXTURES
548	550
33.1	49.2
768	766
620	565
148	201
141	184
146	187
157	245
10	35
4	12
1800	2700
(11.4)	(10.7)
	AND $1H_2:1C_2H_4$. 548 33.1 768 620 148 141 146 157 10 4 1800 (11.4)

proximate calculations indicate that the value of k_2 may be somewhat less in these mixtures. Thus, the most favorable view that could be taken would be that the whole pressure drop is due to ethane formation. The corresponding calculation of k_2 gives 11.4×10^{-7} for the $2H_2:1C_2H_4$ mixture, and 10.7×10^{-7} for the $1H_2:1C_2H_4$ mixture, as compared with 15.1×10^{-7} for the $3H_2:1C_2H_4$ mixture.

Experiments with the reaction vessel filled with broken Pyrex glass (4-10 mesh) are recorded in Table III. Analysis showed that in all cases there was a marked loss of hydrogen in excess of ethane formed. In this case also it is not possible to give precise values of k_2 . Assuming that the whole pressure drop represents reaction, the values of k_2 would be 4.15×10^{-7} at 500° and 1 atm. (initial), and 27.4×10^{-7} at 550° and 1 atm. (initial). These are to be compared with 2.37×10^{-7} , and $15 1 \times 10^{-7}$, respectively,

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in the empty tube. The constants for the packed tube are nearly twice those for the empty tube. Even if this were all due to increased wall reaction in the packed tube, it would still not be serious since the wall surface has been increased by a factor of ten at least. However, the results of analysis show clearly that twice as much hydrogen as ethylene has disappeared, which accounts for the large apparent value of k_2 . In the experiment at 550° the final reaction mixture was fractionated before analysis. The result proved that ethane, rather than a mixture of methane and propane (say), was produced.

TABLE	III
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REACTION OF 3H2:1C2H4 MIXTURE I	n Packed	REACTION	Vessel
Temp., °C.	499	550	550
Initial press. H ₂ , mm.	564	563	335
Initial press. C ₂ H ₄ , mm.	193	193	115
Initial total press., mm.	757	756	450
Final total press., mm.	694	648	390
Pressure drop, mm.	63	108	60
C ₂ H ₆ formed, mm.	45	83	39
H ₂ reacted, mm.	72	126	68
C ₂ H ₄ reacted, mm.	38	65	31
Reaction time, sec.	1800	600	900
$k \times 10^{7}$	(4.15)	(27.4)	(27.3)

Discussion

The results show that the formation of ethane from ethylene and hydrogen is a homogeneous, second-order reaction, at least when hydrogen is in excess. It remains to calculate the reaction rate on the basis of the collision theory.

The values of k_2 for the runs at one atmosphere in the empty bulb with a $3H_2:1C_2H_4$ mixture are fitted by the equation

$$\log_{10} k_2 = -\frac{43,150}{2.303RT} + 5.576$$

as shown by the data of Table IV.

TABLE IV COMPARISON OF CALCULATED AND OBSERVED VALUES OF k_2 $k_1 \times 10^7$ Temp., Å. Obs. Calcd. 748 1.00 0.97773 2.372.45797 5.425.70 825 15.114.5

According to the collision theory, the rate of reaction in terms of molecules of ethane formed per cc. per second should be

$$\alpha\beta 2\sqrt{\frac{2\pi RT(M_1+M_2)}{M_1M_2}}\sigma_{12}^{2}n_1n_2e^{-43,150/RT}$$

where M_1 is the molecular weight of H_2 , M_2 is the molecular weight of C_2H_4 , σ_{12} is the average diameter of H_2 and C_2H_4 in cm., n_1 is the number of mols. of H_2 per cc. and n_2 is the number of mols. of C_2H_4 per cc. α and β have been already defined. Since σ_{12} can only be approximately estimated in the absence of viscosity determinations at the temperatures of the experiments, it seems best to use the velocity data to calculate $\alpha\beta\sigma_{12}^2$. An estimate of $\alpha\beta$ can then be made by substituting a reasonable value of σ_{12} .

 k_2 represents the pressure in mm. of C_2H_6 formed per second when C_2H_4 and H_2 are at 1 mm. pressure each. At 500° (773 Å.) k_2 is 2.45 \times 10⁻⁷. This corresponds to 3.08×10^9 molecules of C_2H_6 formed per cc. per second. At 550° and 1 mm. pressure there will be 1.25×10^{16} molecules each of H_2 and C_2H_4 per cc. Substituting

$$\frac{3.08 \times 10^{9}}{(1.257 \times 10^{16})^{2}} = \alpha \beta \sigma_{12}^{2} \cdot 2 \sqrt{\frac{2\pi 8.32 \times 10^{7} \times 773 \times 28.0}{24.0 \times 4.03}} \cdot e^{-\frac{43,150}{1.985 \times 773}} \alpha \beta \sigma_{12}^{2} = 4.38 \times 10^{-17}$$

If now we assume that

$$\sigma_{\rm H2} = 1 \times 10^{-8}$$

 $\sigma_{\rm C2H4} = 4 \times 10^{-8}$

 $\sigma_{12}^2 = 4 \times 10^{-16}$

then

whence $\alpha\beta = 0.1$, approximately. Thus, of all collisions between H₂ and C₂H₄ molecules having the requisite energy, about 10% lead to formation of C₂H₆. This is to be compared with 0.05% (1/2000) in the combination of ethylene molecules.

Comparison with Equilibrium Data and Rate of Dissociation of Ethane.—If the velocity constant for the combination of ethylene and hydrogen is k_2 , and the constant for dissociation of ethane is k_1 , the equilibrium constant for the dissociation of ethane

$$K = \frac{p_{C_2H_4}p_{H_2}}{p_{C_2H_6}} = \frac{k_1}{k_2}$$

 $C_2H_6 \rightleftharpoons C_2H_4 + H_2$

The experiments here reported give for k_2 in mm.

$$\log_{10}k_2 = -\frac{43,150}{2.3RT} + 5.576$$

For k_2 in atmospheres, this becomes

$$\log_{10}k_2 = -\frac{43,150}{2.3RT} + 8.457$$

For k_1 , the work of Marek and McCluer³ gives

$$\log_{10}k_1 = -\frac{73,170}{2.3RT} + 15.12$$

Thus

$$\log_{10} K = \log_{10} k_1 - \log_{10} k_2 = -\frac{30,020}{2.3RT} + 6.66$$

Direct measurements of K at $600-700^{\circ}$ give²

$$\log_{10} K = -\frac{31,244}{2.3RT} + 6.31$$

The independent determinations thus confirm one another.

Summary

The combination of ethylene and hydrogen in a Pyrex glass vessel at $475-550^{\circ}$ and one atmosphere pressure has been shown to be a homogeneous, second-order reaction. A calculation based on the collision theory indicates that about 10% of the collisions between ethylene and hydrogen molecules possessing the requisite energy (43,150 cal. per mole) eventually result in formation of ethane.

Combination of equations for the rates of ethane formation and of ethane dissociation gives an equation for the equilibrium constant of the reaction

 $C_2H_6 \rightleftharpoons C_2H_4 + H_2$

in good agreement with that obtained by direct measurement.

PRINCETON, NEW JERSEY

[Contribution from the Chemistry Department of the State University of Iowa]

THE PREPARATION AND PROPERTIES OF IODINE MONOCHLORIDE¹

BY JACOB CORNOG AND R. A. KARGES Received January 4, 1932 Published May 7, 1932

I. Preparation

Old Method.—Iodine monochloride has usually been prepared by leading chlorine over solid iodine.² The crude product thus obtained was distilled; the portion of the distillate forming between 100 and 102° was retained. The distillate was far from pure. Stortenbecker³ obtained iodine monochloride of good quality by repeatedly recrystallizing the distillate in its own mother liquor.

Improvement of the Old Method.—The present authors found that passing a slow stream of chlorine through the system during distillation and collecting the distillate formed between 100 and 101.5° increased the yield from about 35 to about 85% and also improved the quality of the

¹ From a thesis submitted to the Graduate College of the State University of Iowa in partial fulfilment of the requirements for the degree of Doctor of Philosophy, by R. A. Karges, August, 1931.

² Gay-Lussac, Ann. chim., 91, 1 (1814); Serullas, Ann. chim phys., 22, 180 (1833); Harmay, J. Chem. Soc., 26, 815 (1873); ibid., 35, 269 (1879); Thorpe, ibid., 37, 174 (1880); 61, 925 (1892).

³ Stortenbecker, Rec. trav. chim., 7, 152 (1888).

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